



CHALMERS
UNIVERSITY OF TECHNOLOGY

Site Communication in Direct Formation of H_2O over Single-Atom Pd@Au Nanoparticles

Downloaded from: <https://research.chalmers.se>, 2024-03-13 08:09 UTC

Citation for the original published paper (version of record):

Svensson, R., Grönbeck, H. (2023). Site Communication in Direct Formation of H_2O over Single-Atom Pd@Au Nanoparticles. *Journal of the American Chemical Society*, 145(21): 11579-11588.
<http://dx.doi.org/10.1021/jacs.3c00656>

N.B. When citing this work, cite the original published paper.

Site Communication in Direct Formation of H₂O₂ over Single-Atom Pd@Au Nanoparticles

Rasmus Svensson* and Henrik Grönbeck*

Cite This: *J. Am. Chem. Soc.* 2023, 145, 11579–11588

Read Online

ACCESS |



Metrics & More

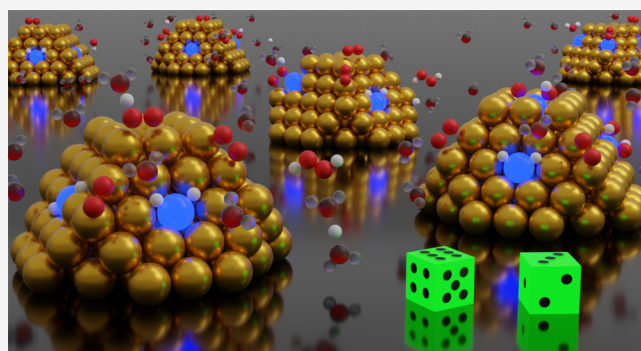


Article Recommendations



Supporting Information

ABSTRACT: Single atom alloy catalysts offer possibilities to obtain turnover frequencies and selectivities unattainable by their monometallic counterparts. One example is direct formation of H₂O₂ from O₂ and H₂ over Pd embedded in Au hosts. Here, a first-principles-based kinetic Monte Carlo approach is developed to investigate the catalytic performance of Pd embedded in Au nanoparticles in an aqueous solution. The simulations reveal an efficient site separation where Pd monomers act as active centers for H₂ dissociation, whereas H₂O₂ is formed over under-coordinated Au sites. After dissociation, atomic H may undergo an exothermic redox reaction, forming a hydronium ion in the solution and a negative charge on the surface. H₂O₂ is preferably formed from reactions between dissolved H⁺ and oxygen species on the Au surface. The simulations show that tuning the nanoparticle composition and reaction conditions can enhance the selectivity toward H₂O₂. The outlined approach is general and applicable for a range of different hydrogenation reactions over single atom alloy nanoparticles.



INTRODUCTION

Hydrogen peroxide (H₂O₂) is an important industrial chemical with mild oxidizing properties and low environmental impact with only H₂O and O₂ as side products during oxidation.¹ The area of usage ranges from bleaching and wastewater treatment to organic synthesis.^{2–4} H₂O₂ is currently produced by sequential reduction and oxidation of anthraquinones.¹ The anthraquinone process has a high selectivity toward H₂O₂; however, it requires large-scale facilities, is energy demanding, involves complicated liquid–liquid extractions, and produces toxic wastes. It is therefore desirable to replace the anthraquinone process with a process where H₂ and O₂ react directly to form H₂O₂. A direct process has the potential to be operated at small scale and to be cost and energy efficient.^{5,6}

Direct synthesis of H₂O₂ occurs via sequential addition of hydrogen to O₂. Scission of the O–O bonds leads to irreversible formation of water and should be avoided.^{7,8} Different mechanisms for direct H₂O₂ formation over metal nanoparticles (NPs) have been discussed in the literature.^{9,10} The mechanisms are sketched in Figure 1. The left reaction cycle shows H₂O₂ formation via a Langmuir–Hinshelwood mechanism. H₂ in this mechanism is adsorbed dissociatively, forming atomic H* on the surface. H* is added sequentially to molecularly adsorbed O₂ forming H₂O₂. The right reaction cycle shows H₂O₂ formation where protons are transferred to the adsorbed O₂ via the solution⁹ or alternatively ligands coating the metal NP.¹¹ It is clear that a combination of the two mechanisms could apply. The side reactions (red arrows)

lead to the unwanted formation of water, as O–O scission is virtually irreversible. Given the reaction cycles, a desirable catalyst for direct H₂O₂ formation should dissociate H₂ and interact strongly enough with O₂ to promote adsorption without O–O bond rupture. Different transition metal catalysts have been investigated for direct H₂O₂ formation, including Pd^{7,12,13} and Au^{5,14,15} NPs. High rates for H₂O₂ formation have been reported over Pd catalysts, however, with low selectivity due to the irreversible O–O bond scission and the subsequent water formation.^{5,15,16} Thus, the interaction between Pd and oxygen is too strong. One possibility to reduce the interaction between Pd and oxygen is to coat the metal with ligands.¹¹ Another option to enhance the selectivity is to alloy Pd with a less reactive metal such as Au. Experiments have shown that it is possible to obtain high yields and high selectivity for H₂O₂ by alloying Pd with Au.^{15,17} The reason for the improved selectivity compared to Pd has been assigned to the suppression of active sites⁵ and geometric effects.¹⁸ It has recently been shown that selectivities approaching 100% can be obtained in the dilute limit of single Pd monomers

Received: January 17, 2023

Published: May 16, 2023



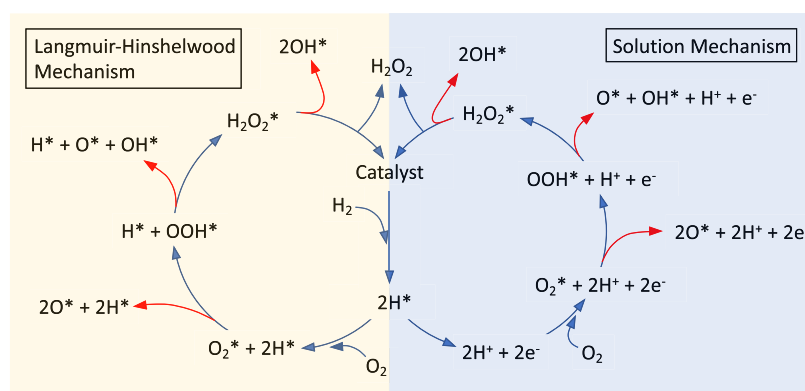


Figure 1. Proposed mechanisms for direct formation of H_2O_2 from O_2 and H_2 over metal nanoparticles. The left cycle shows H_2O_2 formation via a Langmuir–Hinshelwood mechanism, whereas the right cycle shows H_2O_2 formation via the solution or ligands.

embedded in a Au host.¹⁸ The Pd–Au alloy composition generally depends on the manufacturing method.^{15,19,20} In the case of dilute alloys, the distribution of Pd monomers has been measured to be close to random with a large fraction residing close to Au edges.²⁰

The mechanistic understanding of hydrogen transfer reactions over dilute alloys of Pd monomers in Au (Pd@Au) is based on density functional theory calculations performed on extended surfaces.^{18,21–23} These studies have explored reaction paths over the Pd monomers and the possibility to enhance the selectivity by embedding one active site in an inert surface. However, technical catalysts are based on supported NPs, which differ with respect to extended surfaces, as they include a large number of different sites. (Roughly 15% of the surface atoms on a typical 7 nm particle are edge and corner sites.) Understanding the reaction mechanisms and the kinetic behavior over nanoparticles would potentially enable design of catalysts with improved performance. Here, we investigate the direct formation of H_2O_2 from O_2 and H_2 over Pd@Au nanoparticles, which are compared with extended surfaces. The potential energy landscapes for the reaction over a range of different Au and Pd@Au systems are mapped by density functional theory calculations, taking the effect of an aqueous solution into account. The reaction kinetics over NPs are modeled using scaling relation kinetic Monte Carlo simulations including both the Langmuir–Hinshelwood mechanism and solution mechanism (Figure 1). The kinetic Monte Carlo simulations are used to identify the dominant reaction mechanism as a function of NP composition and reaction conditions. We find that Pd monomers embedded in Au(111) have a close to 100% selectivity toward H_2O_2 . Dissociated H on the metal surface undergoes an exothermic redox reaction with water to form water-solvated hydronium ions over a negatively charged metal surface. The presence of under-coordinated Au sites on NPs has a positive effect on the selectivity thanks to an efficient separation of sites that dissociate H_2 (Pd) and adsorb O_2 (Au). The facile intersite communication makes the selectivity over NPs sensitive to the number and distribution of Pd monomers. The simulated kinetic behavior is in good agreement with available experimental data and uncovers mechanisms that could be used to further improve the catalytic performance of dilute alloys. The simulations stress the need to account for the complete potential energy landscapes of solvated NPs to properly describe the kinetic behavior. The outlined approach

is general and applicable for a range of different hydrogenation reactions.

COMPUTATIONAL APPROACHES

Electronic Structure Calculations. Electronic structure calculations are performed using the Vienna Ab initio Simulation Package (VASP).^{24–28} The interaction between the core and valence electrons is described using the projector augmented-wave method.^{28,29} The considered valence electrons are $1s^1$ for H, $2s^2 2p^4$ for O, $5s^0 4d^{10}$ for Pd, and $6s^1 5d^{10}$ for Au. The exchange–correlation functional proposed by Perdew, Burke, and Ernzerhof³⁰ is used together with the Grimme-D3 correction,^{31,32} to capture the van der Waals interactions. The plane waves are truncated at an energy of 450 eV in the expansion of the Kohn–Sham orbitals. Energies are considered to be converged when the change in electronic energy and Kohn–Sham eigenvalues between two succeeding electronic iterations is smaller than 1.0×10^{-5} eV. Structures are regarded to be converged when the forces on all cores are smaller than 0.03 eV/Å. The lattice constant and cohesive energy of Au are calculated to be 4.10 Å and -3.69 eV, respectively, which is in good agreement with the experimental results of 4.08 Å and -3.79 eV, respectively.³³

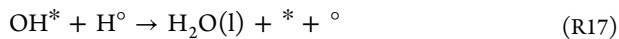
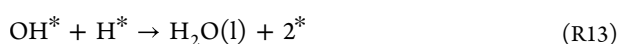
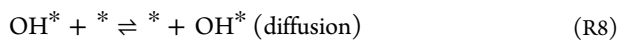
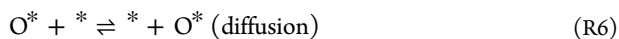
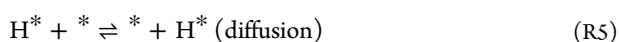
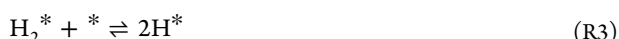
To model the surfaces and NPs, adsorption energies, transition state energies, and vibrational modes are calculated using (3×3) surface cells for Pd@Au(111), Pd@Au(100), Pd@Au(211), and Au(211). The lattice constant of Au is used for the highly diluted Pd@Au systems.³⁴ The surfaces are described by four atomic layers where positions of atoms in the two bottom layers are kept fixed to emulate a bulk system. The surface slabs are separated by 14 Å of vacuum. The Brillouin zone for the surface calculations is sampled with a $(7 \times 7 \times 1)$ k -point mesh using the Monkhorst–Pack scheme.³⁵ The reference energies and vibrational modes of gaseous O_2 and H_2 are calculated using a (14, 15, 16) Å box. The solvation energies of H_2O and H_2O_2 are calculated using a water-filled cubic box with length 8.43 Å and a H_2O density of 1 g/cm³. The vibrational modes are approximated as harmonic oscillators and calculated using finite differences. Transition states for the considered elementary reactions are obtained using the climbing image nudged elastic band (CI-NEB) method.^{36,37}

To capture the influence of the aqueous solution, a water layer is added to all surface–adsorbate structures. Structures are relaxed from the lowest energy configurations originating from a 5 ps molecular dynamics simulation performed at 300

K. Adsorption energies are in this case calculated with respect to the surfaces with a water layer. Constrained molecular dynamics is performed to investigate the transfer of protons from the surface to the solution (Figure 1).

Kinetic Monte Carlo Simulations. The kinetic behavior of direct H₂O₂ formation over NPs and extended surfaces is explored using kinetic Monte Carlo (kMC) simulations. The kMC method is a stochastic approach, which allows for explicit consideration of different types of catalytic sites.^{38–40} The possibility to treat different sites is crucial to describe reactions over alloy particles, with different structural and chemical sites.

The considered reaction events (Figure 1) for H₂O₂ and H₂O formation are



In the reaction network, * and ° denote a surface and solution site, respectively. The kMC simulations are performed using coarse-grained sites; that is, one combined geometric site is used to describe top, bridge, and hollow sites. For the extended surfaces, the turnover frequency and selectivity are simulated using a 20 × 20 lattice with periodic boundary conditions. The reactions over nanoparticles are simulated using truncated octahedra, with diameters of about 2.7 nm.

The kMC simulations are performed using the first reaction method.^{41,42} In the first reaction method, a list of time of occurrences, $t_{\beta,\alpha}$ is calculated for all possible events that

transfer the system from a current state α to a future state β . The time of occurrence is calculated according to

$$t_{\beta,\alpha} = t - \frac{1}{k_{\beta,\alpha}} \ln u \quad (1)$$

where $k_{\beta,\alpha}$ is the rate constant of the considered event and u is a random number from a uniform distribution in the interval (0, 1). The time and system are evolved by performing the event with the shortest time of occurrence. After the execution of an event, time of occurrences are calculated for events that are enabled, whereas events that are disabled are removed from the list of events.

Adsorption steps are considered to be barrierless with rate constants described by collision theory:

$$k_{\text{ads}} = \frac{pAs_0}{\sqrt{2\pi mk_B T}} \quad (2)$$

where p is the partial pressure of the gas, A is the area of the adsorption site, and s_0 is the sticking coefficient at zero coverage. Experimental results for Pd-only systems are used to approximate the sticking coefficients of H₂ and O₂ on the Pd monomers. The sticking coefficients have been measured to be similar for the two gases, being 0.6 on Pd(111)^{43–45} and 0.8 on Pd(100).^{45–47} The sticking coefficient for Pd(100) is used also for Pd@Au(211).

Thermodynamic consistency for reversible reactions is ensured by calculating the desorption rate constant from the equilibrium constant.

$$K = \frac{k_{\text{ads}}}{k_{\text{des}}} = \exp\left\{\frac{-\Delta G}{k_B T}\right\} \quad (3)$$

where ΔG is the Gibbs free energy difference between initial and final states. The reaction rate constants are calculated from transition state theory:

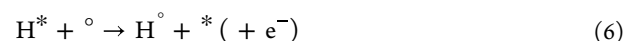
$$k = \frac{k_B T}{h} \frac{Q^\ddagger}{Q} \exp\left\{\frac{-\Delta E^\ddagger}{k_B T}\right\} \quad (4)$$

where ΔE^\ddagger is the zero-point-corrected energy difference between the transition state and the initial state. Q^\ddagger and Q are the partition functions for the transition state (excluding the reaction coordinate) and the initial state, respectively. For the gas phase molecules, the partition function is expressed as the product between the translational, rotational, and vibrational partition functions. The partition functions for adsorbed species are treated as frustrated vibrations, i.e.,

$$Q = \prod_i \frac{1}{1 - \exp\left\{\frac{-\varepsilon_i}{k_B T}\right\}} \quad (5)$$

where ε_i is the energy of vibrational mode i . Modes with energies lower than 12.4 meV (100 cm^{−1}) are set to 12.4 meV due to the anharmonic behavior and computational uncertainties of such modes.

The considered reaction network for direct formation of H₂O₂ involves events and sites that require special attention, namely, the influence of the aqueous solution, the description of reactions over undercoordinated sites, and events that are very fast. The elementary reactions involved in the solution mechanism (Figure 1)



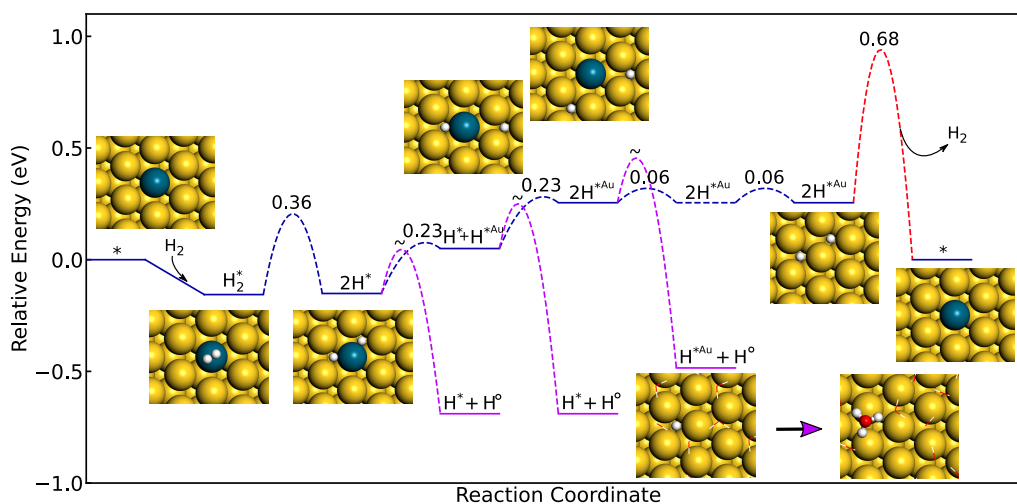


Figure 2. Reaction mechanism for hydrogen dissociation and diffusion over Pd@Au(111). The corresponding adsorption and dissociation energies over Pd@Au(100) and Pd@Au(211) are shown in the SI. * denotes a surface site, and H° denotes a solated proton.

are studied using constrained molecular dynamics (* and ° denote a surface and a solution site, respectively). The mechanism involves proton desorption from the surface with the subsequent formation of a hydronium ion in the water layer and an excess electron in the surface. The molecular dynamics simulations reveal that the barrier for the proton desorption is low (see Supporting Information (SI)), which is in agreement with previous calculations for proton transfer to small H₂O clusters on Au(111).⁴⁸ The rate for proton desorption is therefore dominated by the probability of the water layer to be oriented in a way that can accommodate the desorbed proton. The structural relaxation time of water close to a metal surface is about 2 ns,⁴⁹ which is considerably slower than the structural relaxation time in bulk water (~5 ps). The prefactor of the proton–electron transfer is, thus, set to $0.5 \times 10^9 \text{ s}^{-1}$. The reaction network contains several steps that involve water restructuring (R13–R20). The prefactors for all proton transfer reactions are set to $0.5 \times 10^9 \text{ s}^{-1}$, whereas the prefactor for H₂O₂ desorption is set to $1 \times 10^9 \text{ s}^{-1}$. Equation 3 is used to maintain thermodynamic consistency also in these reactions. The existence of protons in the water solution is accounted for using an explicit site (° in the reaction network). As the diffusion of protons in water is significantly faster than all considered events,⁵⁰ the explicit solution site is connected to all surface sites. The solution is set to have pH = 7, which limits the number of excess protons in the solution. Over the periodic (3 × 3) surface, desorption of one proton to the solution is exothermic, whereas the desorption of a second proton is endothermic when the water is described by one layer. We limit the number of excess protons in the solution to four in the kMC simulations over the (20 × 20) surface lattice and the NPs. The results are not sensitive to the allowed number of excess protons, as demonstrated by explicit simulations for Pd embedded in a (111) facet of an NP allowing for two and eight excess protons.

Scaling relations based on generalized coordination numbers are used to describe the energetic landscape for O₂, O, OH, and OOH species on Au NPs.^{51,52} The generalized coordination number⁵¹ of atom *i* is defined as⁵²

$$\text{GCN}_i = \frac{1}{\text{CN}_{\max}} \sum_{j=1}^{n_i} \text{CN}_j \quad (7)$$

where n_i is the number of nearest neighbors, CN_j is the coordination number of neighbor *j*, and CN_{\max} is the maximum coordination number for the specific atom or group of atoms. The scaling relations for the adsorption energies are obtained by considering a series of model structures. A complete list of model structures, generalized coordination numbers, and adsorption energies is given in the SI.

A general complication in kMC simulations is the large separation in rates for different reactions. For direct H₂O₂ formation over Pd@Au nanoparticles, the O₂ adsorption and desorption events are considerably more frequent than other events. The adsorption/desorption of O₂ is therefore treated in a probabilistic mean-field approach. The O₂ coverage is described implicitly, where empty Au sites are assigned an occupancy based on the equilibrium constant for the considered site. The probability (coverage) of having O₂ adsorbed on a specific site is in this approach given by

$$\theta_{\text{O}_2} = \begin{cases} 0, & \text{if the site is occupied by another adsorbate} \\ \frac{K}{1 + K}, & \text{if the site is unoccupied} \end{cases} \quad (8)$$

RESULTS AND DISCUSSION

The considered Pd@Au NPs are systems with a range of different sites and consequently a complex potential energy landscape. Different strategies are therefore used to describe the potential energy landscape. The adsorption and transition state energies are calculated explicitly over Pd monomers embedded in the Au host, whereas the complete energy landscape over Au NPs is described using scaling relations based on generalized coordination numbers.⁵¹ The use of scaling relations is an efficient approach to obtain the potential energy landscape for the multitude of different sites on an NP.⁵³

Potential Energy Landscapes for H₂O₂ Formation.

The first crucial step in the reaction is H₂ dissociation and H diffusion. The corresponding potential energy landscape over Pd@Au(111) is shown in Figure 2. H₂ adsorbs with an adsorption energy of 0.16 eV. Dissociation into atomic H

residing in fcc-hollow sites is associated with a barrier of 0.36 eV. The dissociated H may thereafter diffuse away from the Pd monomer, with a barrier of 0.23 eV, or undergo a strongly exothermic redox reaction, where a proton desorbs into the water solution while leaving a delocalized excess electron on the surface. The energetics of the redox reaction depends weakly on whether the process occurs close to or far from a Pd monomer [see SI for desorption from Au(111), Pd@Au(111), and Pd(111)]. The diffusion barrier for H over the Au(111) surface is 0.06 eV. Despite the fact that adsorbed H is endothermic with respect to gas phase H_2 , H–H association is associated with a high barrier (0.68 eV). H will therefore remain on the Au(111) surface at relevant temperatures or desorb as a proton to the water solution. The only viable path for H_2 desorption is recombination over the Pd monomers. The state with a proton in the solution (in the form of H_3O^+) and an excess electron on the surface is exothermic and accessible because of the facile H_2 dissociation over Pd monomers, the low adsorption energy of H, and the high electronegativity of Au(111). As the process is exothermic, the metal particles are slightly negatively charged during the reaction. This is in agreement with experimental findings where the reaction is reported to produce a reducing potential for metal particle catalysts.⁵⁴

The potential energy landscapes for H_2O_2 formation over Pd embedded in Au(111), Au(100), and Au(211) via the solution route are shown in Figure 3. The corresponding energies for H_2O_2 formation via the Langmuir–Hinshelwood mechanism over Pd@Au(111) and Pd@Au(211) are reported in the SI.

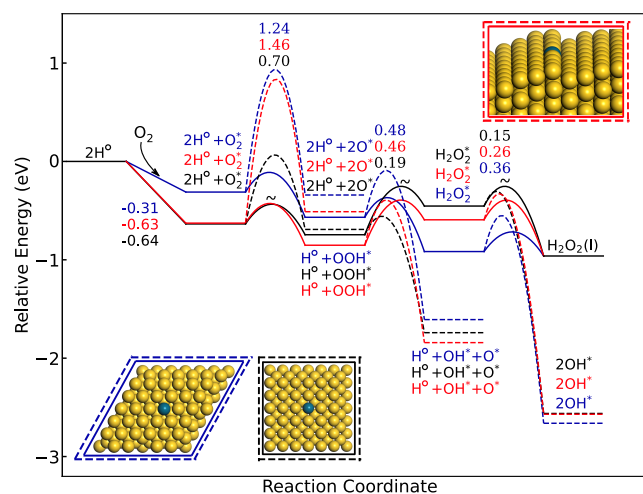


Figure 3. Potential energy landscape for the formation of H_2O_2 and side reactions forming H_2O over Pd@Au(111) (blue), Pd@Au(100) (black), and Pd@Au(211) (red). * denotes a surface site and H^+ denotes a solvated proton.

The reference state in Figure 3 is a bare surface with two protons in the solution ($2H^+$). The adsorption energy of O_2 depends on whether H^+ is adsorbed at the Pd site, and we consider in Figure 3 the case with zero H^+ coverage. The adsorption of O_2 is influenced by the presence of water, which facilitates a metal to O_2 charge transfer (see the SI). The dissociation of O_2^* is prevented by high barriers. The formation of OOH^* is exothermic over all three surfaces. The subsequent formation of $H_2O_2^*$ is, however, only exothermic over Pd@Au(111). Dissociation of OOH^* is

competitive with the endothermic formation of $H_2O_2^*$ over Pd@Au(100) and Pd@Au(211). Note that the formation of OOH^* and $H_2O_2^*$ are reversible, owing to the high stability of the proton in the solution. This is in variance with the Langmuir–Hinshelwood path (SI), where both OOH^* formation and $H_2O_2^*$ formation are exothermic and the barriers for the backward reactions are substantial. The potential energy landscapes for Pd@Au(100) and Pd@Au(211) have local minima at OOH^* and a proton in the solution, which is preferred with respect to $H_2O_2^*$. Thus, the potential energy landscapes indicate that the selectivity is lower over Pd@Au(100) and Pd@Au(211) compared to Pd@Au(111). $H_2O_2^*$ desorption competes with irreversible $H_2O_2^*$ dissociation forming $2OH^*$. The dissociation barrier is highest on Pd@Au(111) and lowest on Pd@Au(100). We find that the potential energy landscapes over Pd@Au(100) and Pd@Au(211) are similar; both systems bind H_2^* , H^* , O_2^* , and OOH^* stronger than does Pd@Au(111) and have lower barriers for OOH^* and $H_2O_2^*$ dissociation.

Owing to the facile H diffusion over gold surfaces (H^*) and proton diffusion via the water solution (H^+), it is possible to form OOH^* and H_2O_2 from adsorbed O_2 on undercoordinated Au sites. Scaling relations are used to describe the energy landscape over Au sites. The potential energy landscape for H_2O_2 formation over Au(211) together with scaling relations are shown in Figure 4. The dissociation barriers of O_2^* and OOH^* are high, and $H_2O_2^*$ desorbs once formed. The formations of OOH^* and H_2O_2 are both exothermic over Au(211), which indicates that the reaction could occur on undercoordinated sites. The exothermicity in the formation of the intermediates changes with generalized coordination number, as the scaling is different for O_2^* and OOH^* .

Kinetic Monte Carlo Simulations. Kinetic Monte Carlo simulations are used to investigate turnover frequencies (TOF) and selectivities (S) for direct H_2O_2 formation over different Pd@Au structures. Simulations are performed to explore the effects of reaction conditions (temperature and pressure) as well as the effect of the number and placement of Pd monomers. The TOF is defined as the number of H_2O_2 (or H_2O) formed per Pd monomer and second. The reaction takes place in a water solution, which implies that adsorption of H_2O on the Pd monomer may block the site for H_2 and O_2 adsorption. The adsorption and desorption of H_2O on the Pd site are fast processes, which we include by scaling the TOFs with a Boltzmann distribution determined by the adsorption energy of H_2O on the Pd monomer from the water solution. The selectivity is given by

$$S = \frac{\text{TOF}(H_2O_2)}{\text{TOF}(H_2O) + \text{TOF}(H_2O_2)} \quad (9)$$

Influence of Temperature. The temperature dependence of TOFs and selectivities is shown in Figure 5 for Pd embedded in Au(111), Au(100), and Au(211), as well as the corresponding positions in a 2.7 nm truncated octahedron. We denote the systems with extended surfaces Pd@Au(111), Pd@Au(100), and Pd@Au(211), whereas the NP systems are denoted Pd@NP(111), Pd@NP(100), and Pd@NP(edge). The partial pressures of H_2 and O_2 are set to 100 kPa for all simulations in Figure 5.

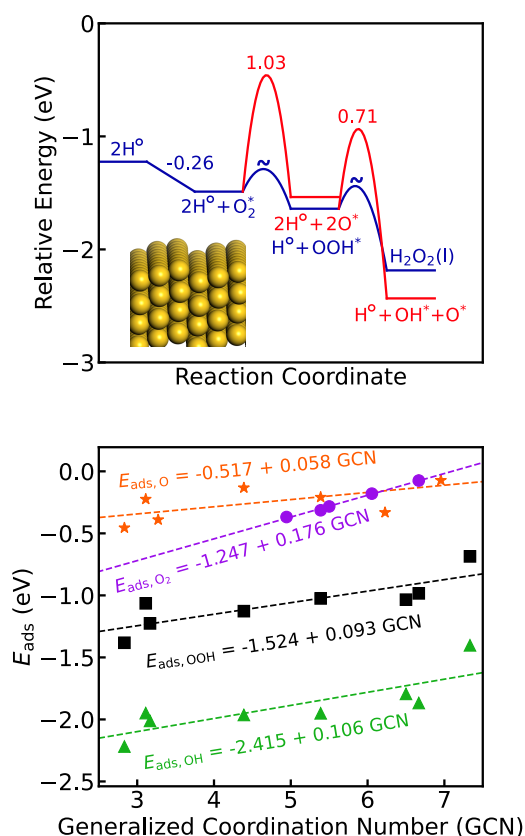


Figure 4. Top: The potential energy landscape for the formation of H_2O_2 and competing side reactions over $\text{Au}(211)$. * denotes a surface site and H° denotes a solvated proton. Bottom: Non-zero-point-corrected scaling relations to describe adsorption energies on undercoordinated Au NP sites. The scaling relations have mean absolute errors of 0.086 eV for O^* , 0.0062 eV for O_2^* , 0.11 eV for OOH^* , and 0.082 eV for OH^* .

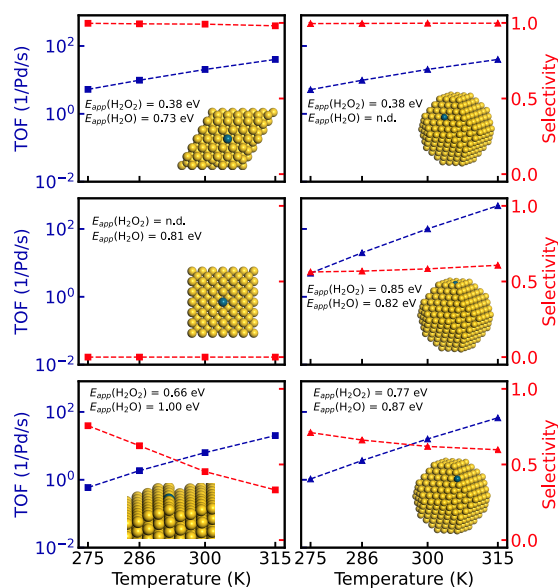


Figure 5. Turnover frequency of H_2O_2 (blue) and selectivity (red) as a function of temperature, in the interval 275–315 K over Pd@111, Pd@100, Pd@step, Pd@NP(111), Pd@NP(100), and Pd@NP(edge). The partial pressures of H_2 and O_2 are set to 100 kPa. The standard deviations are taken over 30 independent simulations.

The selectivity over Pd@111 is close to 100% in the entire temperature interval, which is also the case for a Pd monomer placed in the Au(111) facet of the truncated octahedron [Pd@NP(111)]. Importantly, however, the mechanism for H_2O_2 formation over Pd@111 is significantly different compared to Pd@NP(111). H_2O_2 is on Pd@111 formed exclusively over the Pd monomer, whereas more than 95% of H_2O_2 is formed over undercoordinated Au edge and corner sites in the case of Pd@NP(111). The reason for similar TOFs is that H_2 dissociation occurs only on the Pd monomer, which has the same properties on Pd@111 and Pd@NP(111). The high selectivity for the two systems is in both cases thanks to a high OOH^* dissociation barrier.

Placing Pd in the extended (100)-surface has dramatic effects on the H_2O_2 formation. The TOF and selectivity toward H_2O_2 is zero for Pd@100, which is a consequence of facile OOH^* and H_2O_2^* dissociation. A reasonable selectivity (around 60%) is instead predicted for Pd@NP(100), despite the fact that the selectivity is zero for Pd@100. The difference between the extended surface and the NP is again traced to different mechanisms. H_2O_2 is for the NP formed via the solution mechanism over undercoordinated Au sites, which have considerable barriers for OOH^* dissociation. H_2O is on Pd@NP(100) instead formed over the Pd site; thus the two products are formed over different sites. The selectivity is not as high as on Pd@NP(111) because of the reversibility of the OOH^* formation on the undercoordinated Au sites; the barrier for OOH^* decomposition to O_2^* and H° is low.

To investigate the effect of placing the Pd monomer in a step, we consider Au(111) with a Au(211) step [Pd@step]. Despite similar potential energy landscapes over the Pd monomer embedded in Au(100) and Au(211) (see Figure 3), the kinetic behavior is different. The selectivity is about 50% over Pd@step, which is a consequence of undercoordinated Au sites where O_2 can adsorb and form H_2O_2 . The reason for the limited selectivity is the low coverage and concentration of H ; thus OOH^* may decompose to OH^* and O^* before H_2O_2^* is formed. The performance of Pd@NP(edge) is similar to Pd@step, and the solution mechanism is the dominant reaction path. Despite that the number of undercoordinated Au sites is much higher on the NP compared to Pd@step, the selectivity on the Pd@NP(edge) is not markedly higher than on the Pd@step. A similar selectivity arises as the OOH^* decomposition to O_2^* and H° is more facile on the NP edges and corners than on the Pd@step.

Influence of Pressure. Besides temperature, the kinetic behavior could be modified with the reactant pressures. The selectivities over the different structures as a function of $p(\text{H}_2)/p(\text{O}_2)$ ratio are shown in Figure 6.

For Pd@111 and Pd@NP(111), the selectivity is close to 100%, with a weak dependence on $p(\text{H}_2)/p(\text{O}_2)$ ratio. The high selectivity is connected to the large barriers for O–O bond rupture. For Pd@111, H_2O_2 is formed exclusively over the Pd monomer, whereas H_2O_2 is formed both over Pd@Au(111) and undercoordinated Au sites over Pd@NP(111).

Similar to the temperature dependence, the selectivity is close to zero over a Pd monomer located in the extended Au(100) surface regardless of the partial pressure ratio. The reason for the low selectivity is the high rate for OOH^* dissociation compared to the formation rate of H_2O_2^* . The

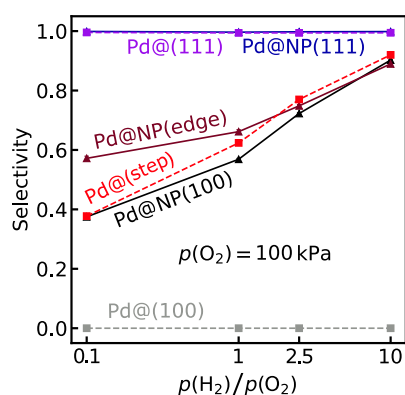


Figure 6. Selectivity toward H_2O_2 as a function of $p(\text{H}_2)/p(\text{O}_2)$ ratio, over Pd@(111), Pd@(100), Pd@step), Pd@NP(111), Pd@NP(100), and Pd@NP(edge). All simulations are performed at 286 K. The standard deviations are taken over 30 independent simulations.

ratio of the partial pressures has, instead, an effect when the Pd monomer is placed in a (100) facet of an NP. An alternative reaction route is enabled on the NP, as H_2O_2 can form over undercoordinated Au edge and corner sites, where the barriers for O–O scission are higher than over the Pd@Au(100). The selectivity approaches 100% at high $p(\text{H}_2)/p(\text{O}_2)$ ratio, as H_2 excess effectively blocks the Pd monomer and prevents O_2 adsorption, hence hindering OOH^* formation and dissociation. Moreover, a high H_2 pressure increases the amount of water-solvated protons in the system (the solution site has a coverage of about 10^{-3} per NP for NPs where the Pd monomers are located in the (111) facets), which results in shorter lifetimes of OOH^* and higher H_2O_2 formation rates. The increased concentration of protons in the solution at higher H_2 pressures agrees with experimental findings for the reaction over PtAu₆₀ NPs.⁵⁴

The dependence on the pressure ratio for Pd@step) and Pd@NP(edge) is similar to Pd@NP(100); an increased $p(\text{H}_2)/p(\text{O}_2)$ ratio yields higher selectivity. The improved selectivity with H_2 excess is again thanks to hydrogen blocking of the Pd monomer, which suppresses O_2 adsorption on the Pd site. The difference in selectivity for Pd@step) and Pd@(100) is not directly evident from the potential energy landscapes for the two Pd monomers in Figure 3. The underlying reason is that Pd@step) contains undercoordinated Au sites where H_2O_2 can be formed; hence the formation of H_2O_2 on Pd@step) is not limited to the Pd monomer as is the case for Pd@(100). Generally, the selectivity toward H_2O_2 is favored by high H_2 and low O_2 pressures.

Effect of Multiple Pd Monomers. To elucidate the governing mechanisms for H_2O_2 selectivity and the effect of the number and location of Pd monomers, the steady state net rates over Au and Pd sites for selected reaction steps are presented in Figure 7. The considered NP is a 2.7 nm truncated Au octahedron with Pd monomers placed in (111) and (100) facets as well as in edges. H_2 dissociation determines the TOF over the NP, OOH^* formation shows where the reaction occurs, and H_2O_2 formation determines the selectivity and TOF toward H_2O_2 .

The selectivity over a truncated octahedron with a single Pd monomer is clearly affected by the position of the monomer (compare with Figure 5 and Figure 6), where the selectivity toward H_2O_2 is close to 100% over Pd@NP(111) and

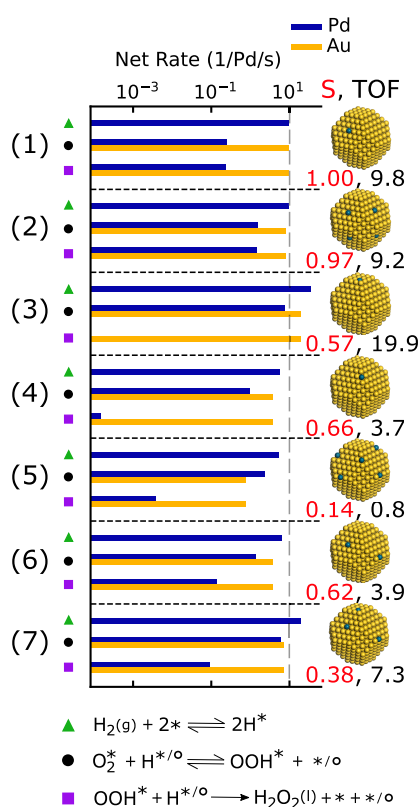


Figure 7. Steady state net rates of H_2 dissociation, OOH^* formation, and H_2O_2 desorption, as well as the selectivity over truncated octahedra with different Pd distributions. All simulations are performed at 286 K and O_2 and H_2 pressures of 100 kPa.

considerably lower when Pd is located at either Au(100) or on an NP edge. The locations of the Pd monomers become even more important when the number of Pd monomers is increased. When one Pd monomer is placed in each (111) facet, the selectivity is still close to 100%. The situation is different with many Pd monomers located in edge sites, where the selectivity toward H_2O_2 is severely decreased with respect to the case with only one Pd monomer. For NPs with Pd monomers located at (111), (100), and edge sites, the selectivity toward H_2O_2 is determined by the Pd monomers in (100) and edge sites.

For an NP with a single Pd monomer in a (111) facet, H_2 is dissociated over the Pd monomer. Owing to the facile H diffusion, the net formation rates of OOH^* and H_2O_2 are dominated by reactions over the undercoordinated Au sites. As the selectivity is almost 100%, the steady state net formation rates of OOH^* and H_2O_2 are equal to the net rate of H_2 dissociation. For an NP where one Pd monomer is placed in each (111) facet, the Au-edge/Pd ratio is decreased, which leads to a higher OOH^* net formation rate over the Pd monomers. However, the net formation rate of H_2O_2 desorption is only slightly reduced compared to the net rate of OOH^* formation over both Au and Pd, thanks to the high selectivity over Pd@Au(111).

When the Pd monomer is placed in either the (100) facet or in an edge, the net formation rate of H_2O_2 is lower than the net rate of H_2 dissociation; thus the selectivity is low. In these cases, the net rates of OOH^* formation over Pd are similar to the net formation rates over Au. The OOH^* species formed over Au yield H_2O_2 , whereas OOH^* formed over Pd results in

H₂O due to facile OOH* scission over these monomers. An increased number of Pd monomers located at edge sites results in a substantial decrease in selectivity toward H₂O₂ as OOH* formation and subsequent O–O bond rupture over Pd is preferred, as compared to OOH* formation over Au.

The NP with a Pd monomer located both in the (111) facet and in an edge does not show increased selectivity compared to the NP with only one Pd monomer located in an edge. A large fraction of OOH* in this case is formed over Pd@Au(edge) rather than over Pd@Au(111). The net rate of H₂O₂ desorption from Pd is low, as OOH* dissociates easily over Pd@Au(edge), which is a consequence of a strong O₂ adsorption energy. The preference of OOH* formation over Pd monomers, where the selectivity is low, is emphasized when an additional Pd monomer is added to the (100) facet. In this case, the steady state net rate of OOH* formation over Pd is similar to Au, whereas the net rate of H₂O₂ is low. The site communication between the different Pd monomers and the undercoordinated Au sites occurs mainly via water-mediated proton transfer. As the H⁺ diffusion in the solution is fast with respect to the surface reactions, the distance between the Pd monomers is not a crucial parameter in our simulations. Owing to the large differences in net formation rates of OOH* over the different Pd monomers, the selectivities over NPs with a larger number of Pd monomers are therefore determined by the worst-positioned Pd monomers that bind O₂ strongly. Thus, the number of Pd monomers per NP should be kept low to obtain high selectivity. We elaborate on the influence of Pd monomer concentration in the SI.

General Observations. DFT calculations and kinetic Monte Carlo simulations have been used to explore direct H₂O₂ formation over Pd@Au alloy structures in an aqueous solution. The requirement for high selectivity toward H₂O₂ is that the catalysts should enable facile H₂ dissociation and adsorption of O₂. The interaction with O₂ should not be too strong as to prevent irreversible O–O bond rupture.

We find that a selectivity close to 100% is obtained when a Pd monomer is embedded in the extended Au(111) surface. H₂O₂ is predominately formed via a mechanism where H⁺ is sequentially added to O₂ via the water solution, rather than the conventional Langmuir–Hinshelwood mechanism. Thus, a crucial step for the high selectivity is the close to barrierless H⁺ desorption into the solution. The desorption process is a redox reaction where the electron is donated to the surface, whereas the proton forms a hydronium ion in the solution. The redox reaction is strongly exothermic thanks to the low adsorption energy of atomic H on Au surfaces and the high electro-negativity of Au. Association of atomic H on the Au surface is unlikely at relevant temperatures, owing to the high recombination barrier. The reaction over Pd@Au(111) is strictly sequential, not only with respect to addition of protons to adsorbed O₂ but also in the adsorption of H₂ and O₂. At least one of the H atoms from dissociated H₂ must leave the Pd monomer before O₂ can adsorb.

Technological implementation of Pd@Au systems requires Pd embedded in Au NPs. NPs are inherently different from extended surfaces thanks to the large number of different sites, including edge and corner sites. For example, 35% of the surface atoms of the studied 2.7 nm truncated octahedron are edges or corners. As O₂ is known to adsorb on undercoordinated Au atoms, NPs enable additional reaction routes. With Pd embedded in Au NPs, it is possible to separate the sites for H₂ and O₂ adsorption. We have studied H₂O₂

formation over Pd monomers embedded in truncated Au octahedra. Placing the Pd monomer in the (111) facet of the NP results in a close to 100% selectivity toward H₂O₂; importantly, however, the reaction landscape and reaction mechanism is different from the extended Au(111) surface. The majority of H₂O₂ is formed over the NP edges, and the solution route is the dominating reaction mechanism also over NPs.

It is experimentally challenging to steer the location of the Pd monomers in the NPs. We find that the selectivity decreases to about 60% if the Pd monomer instead resides in a (100) facet or in an edge of the NP. The reason for the lower selectivity is a stronger adsorption energy of O₂ to a low-coordinated Pd site. Thus, the efficiency of the site-separation for H₂ and O₂ adsorption is reduced. OOH* may form over undercoordinated Pd monomers, which also allow for facile OOH* dissociation. For NPs with multiple Pd monomers, we find that monomers with unfavorable positions determine the selectivity. The lower selectivity over ill-positioned Pd monomers can to some extent be compensated by tuning the reaction conditions. An increased $p(\text{H}_2)/p(\text{O}_2)$ ratio increases the selectivity toward H₂O₂, which is in agreement with experimental results.¹⁸ The higher selectivity originates from H blocking of the Pd monomer, which steers the OOH* formation to undercoordinated Au sites. Our simulations reproduce the experimentally reported¹⁸ dependence on H₂ and O₂ pressure on H₂O₂ formation rate (see SI). The reaction order in H₂ is positive at low pressures and close to zero at high pressures, whereas the reaction order in O₂ is slightly negative in the investigated pressure interval.

The apparent activation energies for H₂O₂ and H₂O formation over an ensemble of NPs have experimentally been reported to be 0.18 and 0.75 eV, respectively.¹⁸ A direct comparison to our results is difficult due to the strong dependence on the number and placement of Pd monomers in the Au NPs; however, Pd positioned in the extended Au(111) could be a reasonable representation. We calculate the apparent activation energies for H₂O₂ and H₂O formation over Pd@Au(111) to be 0.38 and 0.73 eV, respectively. The apparent activation energy for H₂O₂ formation over a Au NP with Pd positioned in a Au(111) facet is also 0.38 eV. The apparent activation energies for both H₂O₂ and H₂O formation increase when Pd is placed in undercoordinated positions. The difference in apparent activation energies between H₂O₂ and H₂O is primarily related to the competing H₂O₂ formation and OOH* dissociation, which may occur on different sites. We find that the H₂ dissociation determines the rate of the reaction, as close to all H on the catalyst surface react to form either H₂O₂ or H₂O.

CONCLUSIONS

We have developed a first-principles-based kinetic Monte Carlo approach to explore the governing factors in direct formation of H₂O₂ over Pd embedded in Au NPs and extended surfaces in a water solution. Whereas a negligible amount of H₂O₂ is formed over pure Au NPs, systems with Pd monomers embedded in Au are active for the reaction. We find that a high activity and selectivity is possible over dilute Pd@Au NPs thanks to an efficient site separation, where H₂ dissociation occurs over Pd sites and O₂ adsorption and hydrogenation occur over Au edges and corners. Atomic H on Au is found to undergo a redox reaction where H⁺ desorbs to the water solution, leaving an electron in the metal. The water solution is

found to mediate the reaction by enabling facile H^+ diffusion. OOH and H_2O_2 are predominantly formed by reactions between O_2 and OOH and dissolved H^+ . The simulations stress the need to account for the complete potential energy landscapes of the solvated NPs to properly describe the kinetic behavior of the reaction. Our results rationalize experimental findings and provide guidelines to design and operate single atom alloy catalysts to obtain high activity and selectivity for a range of different hydrogenation reactions.

■ ASSOCIATED CONTENT

SI Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/jacs.3c00656>.

Constrained molecular dynamics simulations for H^+ diffusion; analysis of energy contributions in the formation of hydronium ions in the water solution; barriers for H_2 dissociation and OOH and H_2O_2 formation over the considered surfaces; data for scaling relations; influence of the number of Pd monomers in the kMC simulations; TOF as a function of partial pressures; analysis of how the charge state of adsorbed O_2 depends on the presence of water (PDF)

■ AUTHOR INFORMATION

Corresponding Authors

Rasmus Svensson – Department of Physics and Competence Centre for Catalysis, Chalmers University of Technology, SE-412 96 Göteborg, Sweden; Email: rassve@chalmers.se

Henrik Grönbeck – Department of Physics and Competence Centre for Catalysis, Chalmers University of Technology, SE-412 96 Göteborg, Sweden; orcid.org/0000-0002-8709-2889; Email: ghj@chalmers.se

Complete contact information is available at: <https://pubs.acs.org/10.1021/jacs.3c00656>

Notes

The authors declare no competing financial interest.

■ ACKNOWLEDGMENTS

Financial support is acknowledged from the Swedish Research Council (2020-05191). The calculations were performed at NSC via a SNIC grant (2022/3-14). The Competence Centre for Catalysis (KCK) is hosted by Chalmers University of Technology and is financially supported by the Swedish Energy Agency and the member companies Johnson Matthey, Perstorp, Powercell, Preem, Scania CV, Umicore, and Volvo Group.

■ REFERENCES

- (1) Campos-Martin, J. M.; Blanco-Brieva, G.; Fierro, J. L. Hydrogen peroxide synthesis: an outlook beyond the anthraquinone process. *Angew. Chem., Int. Ed.* **2006**, *45*, 6962–6984.
- (2) Jones, C. W. *Applications of Hydrogen Peroxide and Derivatives*; Royal Society of Chemistry, 1999; Vol. 2; p 80.
- (3) Pera-Titus, M.; Garcia-Molina, V.; Baños, M. A.; Giménez, J.; Espluga, S. Degradation of chlorophenols by means of advanced oxidation processes: a general review. *Appl. Catal. B: Environ.* **2004**, *47*, 219–256.
- (4) Hage, R.; Lienke, A. Applications of transition-metal catalysts to textile and wood-pulp bleaching. *Angew. Chem., Int. Ed.* **2006**, *45*, 206–222.
- (5) Edwards, J. K.; Solsona, B.; Carley, A. F.; Herzing, A. A.; Kiely, C. J.; Hutchings, G. J. Switching off hydrogen peroxide hydrogenation in the direct synthesis process. *Science* **2009**, *323*, 1037–1041.
- (6) Flaherty, D. W. Direct synthesis of H_2O_2 from H_2 and O_2 on Pd catalysts: current understanding, outstanding questions, and research needs. *ACS Catal.* **2018**, *8*, 1520–1527.
- (7) Dissanayake, D. P.; Lunsford, J. H. The direct formation of H_2O_2 from H_2 and O_2 over colloidal palladium. *J. Catal.* **2003**, *214*, 113–120.
- (8) Plauk, A.; Stangland, E. E.; Dumesic, J. A.; Mavrikakis, M. Active sites and mechanisms for H_2O_2 decomposition over Pd catalysts. *Proc. Natl. Acad. Sci. U. S. A.* **2016**, *113*, E1973–E1982.
- (9) Wilson, N. M.; Flaherty, D. W. Mechanism for the direct synthesis of H_2O_2 on Pd clusters: heterolytic reaction pathways at the liquid–solid interface. *J. Am. Chem. Soc.* **2016**, *138*, 574–586.
- (10) Adams, J. S.; Chemburkar, A.; Priyadarshini, P.; Ricciardulli, T.; Lu, Y.; Maliekkal, V.; Sampath, A.; Winikoff, S.; Karim, A. M.; Neurock, M.; et al. Solvent molecules form surface redox mediators in situ and cocatalyze O_2 reduction on Pd. *Science* **2021**, *371*, 626–632.
- (11) Chen, L.; Moura, P.; Medlin, J. W.; Grönbeck, H. Multiple Roles of Alkanethiolate-Ligands in Direct Formation of H_2O_2 over Pd Nanoparticles. *Angew. Chem., Int. Ed.* **2022**, *61*.
- (12) Samanta, C.; Choudhary, V. R. Direct synthesis of H_2O_2 from H_2 and O_2 and decomposition/hydrogenation of H_2O_2 in an aqueous acidic medium over halide-modified Pd/ Al_2O_3 catalysts. *Appl. Catal. A: General* **2007**, *330*, 23–32.
- (13) Chen, L.; Medlin, J. W.; Grönbeck, H. On the reaction mechanism of direct H_2O_2 formation over Pd catalysts. *ACS Catal.* **2021**, *11*, 2735–2745.
- (14) Landon, P.; Collier, P. J.; Carley, A. F.; Chadwick, D.; Papworth, A. J.; Burrows, A.; Kiely, C. J.; Hutchings, G. J. Direct synthesis of hydrogen peroxide from H_2 and O_2 using Pd and Au catalysts. *Phys. Chem. Chem. Phys.* **2003**, *5*, 1917–1923.
- (15) Edwards, J. K.; Freakley, S. J.; Carley, A. F.; Kiely, C. J.; Hutchings, G. J. Strategies for designing supported gold–palladium bimetallic catalysts for the direct synthesis of hydrogen peroxide. *Acc. Chem. Res.* **2014**, *47*, 845–854.
- (16) Choudhary, V. R.; Samanta, C.; Choudhary, T. Factors influencing decomposition of H_2O_2 over supported Pd catalyst in aqueous medium. *J. Mol. Catal. A: Chemical* **2006**, *260*, 115–120.
- (17) Edwards, J. K.; Carley, A. F.; Herzing, A. A.; Kiely, C. J.; Hutchings, G. J. Direct synthesis of hydrogen peroxide from H_2 and O_2 using supported Au–Pd catalysts. *Faraday Disc* **2008**, *138*, 225–239.
- (18) Ricciardulli, T.; Gorthy, S.; Adams, J. S.; Thompson, C.; Karim, A. M.; Neurock, M.; Flaherty, D. W. Effect of Pd coordination and isolation on the catalytic reduction of O_2 to H_2O_2 over PdAu bimetallic nanoparticles. *J. Am. Chem. Soc.* **2021**, *143*, 5445–5464.
- (19) Casari, C. S.; Foglio, S.; Siviero, F.; Bassi, A. L.; Passoni, M.; Bottani, C. E. Direct observation of the basic mechanisms of Pd island nucleation on Au (111). *Phys. Rev. B* **2009**, *79*, 195402.
- (20) Baber, A. E.; Tierney, H. L.; Sykes, E. C. H. Atomic-scale geometry and electronic structure of catalytically important Pd/Au alloys. *ACS Nano* **2010**, *4*, 1637–1645.
- (21) Lucci, F. R.; Darby, M. T.; Mattera, M. F.; Ivimey, C. J.; Therrien, A. J.; Michaelides, A.; Stamatakis, M.; Sykes, E. C. H. Controlling hydrogen activation, spillover, and desorption with Pd–Au single-atom alloys. *J. Phys. Chem. Lett.* **2016**, *7*, 480–485.
- (22) Thirumalai, H.; Kitchin, J. R. Investigating the reactivity of single atom alloys using density functional theory. *Top. Catal.* **2018**, *61*, 462–474.
- (23) Réocreux, R.; Sykes, E. C. H.; Michaelides, A.; Stamatakis, M. Stick or Spill? Scaling Relationships for the Binding Energies of Adsorbates on Single-Atom Alloy Catalysts. *J. Phys. Chem. Lett.* **2022**, *13*, 7314–7319.
- (24) Kresse, G.; Hafner, J. Ab initio molecular dynamics for liquid metals. *Phys. Rev. B* **1993**, *47*, 558.
- (25) Kresse, G.; Hafner, J. Ab initio molecular dynamics for open-shell transition metals. *Phys. Rev. B* **1993**, *48*, 13115.

- (26) Kresse, G.; Hafner, J. Ab initio molecular-dynamics simulation of the liquid-metal–amorphous-semiconductor transition in germanium. *Phys. Rev. B* **1994**, *49*, 14251.
- (27) Kresse, G.; Furthmüller, J. Efficient iterative schemes for ab initio total-energy calculations using a plane-wave basis set. *Phys. Rev. B* **1996**, *54*, 11169.
- (28) Kresse, G.; Joubert, D. From ultrasoft pseudopotentials to the projector augmented-wave method. *Phys. Rev. B* **1999**, *59*, 1758.
- (29) Blöchl, P. E. Projector augmented-wave method. *Phys. Rev. B* **1994**, *50*, 17953.
- (30) Perdew, J. P.; Burke, K.; Ernzerhof, M. Generalized gradient approximation made simple. *Phys. Rev. Lett.* **1996**, *77*, 3865.
- (31) Grimme, S.; Antony, J.; Ehrlich, S.; Krieg, H. A consistent and accurate ab initio parametrization of density functional dispersion correction (DFT-D) for the 94 elements H–Pu. *J. Chem. Phys.* **2010**, *132*, 154104.
- (32) Grimme, S.; Ehrlich, S.; Goerigk, L. Effect of the damping function in dispersion corrected density functional theory. *J. Comput. Chem.* **2011**, *32*, 1456–1465.
- (33) Lide, D. R. *CRC Handbook of Chemistry and Physics*; CRC Press, 2004; Vol. 85.
- (34) Okamoto, H.; Massalski, T. The Au–Pd (Gold–Palladium) system. *Bulletin of Alloy Phase Diagrams* **1985**, *6*, 229–235.
- (35) Monkhorst, H. J.; Pack, J. D. Special points for Brillouin-zone integrations. *Phys. Rev. B* **1976**, *13*, 5188.
- (36) Mills, G.; Jónsson, H.; Schenter, G. K. Reversible work transition state theory: application to dissociative adsorption of hydrogen. *Surf. Sci.* **1995**, *324*, 305–337.
- (37) Henkelman, G.; Uberuaga, B. P.; Jónsson, H. A climbing image nudged elastic band method for finding saddle points and minimum energy paths. *J. Chem. Phys.* **2000**, *113*, 9901–9904.
- (38) Prats, H.; Illas, F.; Sayos, R. General concepts, assumptions, drawbacks, and misuses in kinetic Monte Carlo and microkinetic modeling simulations applied to computational heterogeneous catalysis. *Int. J. Quantum Chem.* **2018**, *118*, No. e25518.
- (39) Bruix, A.; Margraf, J. T.; Andersen, M.; Reuter, K. First-principles-based multiscale modelling of heterogeneous catalysis. *Nature Catalysis* **2019**, *2*, 659–670.
- (40) Pineda, M.; Stamatakis, M. Kinetic Monte Carlo simulations for heterogeneous catalysis: Fundamentals, current status, and challenges. *J. Chem. Phys.* **2022**, *156*, 120902.
- (41) Jansen, A. P. J. *An Introduction to Kinetic Monte Carlo Simulations of Surface Reactions*; Springer, 2012; Vol. 856; pp 53–54.
- (42) Jørgensen, M.; Grönbeck, H. MonteCoffee: A programmable kinetic Monte Carlo framework. *J. Chem. Phys.* **2018**, *149*, 114101.
- (43) Gostein, M.; Sitz, G. O. Rotational state-resolved sticking coefficients for H₂ on Pd (111): testing dynamical steering in dissociative adsorption. *J. Chem. Phys.* **1997**, *106*, 7378–7390.
- (44) Sjövall, P.; Uvdal, P. Oxygen sticking on Pd (111): double precursors, corrugation and substrate temperature effects. *Chem. Phys. Lett.* **1998**, *282*, 355–360.
- (45) den Dunnen, A.; Wiegman, S.; Jacobse, L.; Juurlink, L. B. Reaction dynamics of initial O₂ sticking on Pd (100). *J. Chem. Phys.* **2015**, *142*, 214708.
- (46) Rettner, C.; Auerbach, D. Search for oscillations in the translational energy dependence of the dissociation of H₂ on Pd (100). *Chem. Phys. Lett.* **1996**, *253*, 236–240.
- (47) Gerbi, A.; Savio, L.; Vattuone, L.; Pirani, F.; Cappelletti, D.; Rocca, M. Role of Rotational Alignment in Dissociative Chemisorption and Oxidation: O₂ on Bare and CO-Precovered Pd (100). *Angew. Chem., Int. Ed.* **2006**, *45*, 6655–6658.
- (48) Pan, M.; Pozun, Z. D.; Yu, W.-Y.; Henkelman, G.; Mullins, C. B. Structure revealing H/D exchange with co-adsorbed hydrogen and water on gold. *J. Phys. Chem. Lett.* **2012**, *3*, 1894–1899.
- (49) Limmer, D. T.; Willard, A. P.; Madden, P.; Chandler, D. Hydration of metal surfaces can be dynamically heterogeneous and hydrophobic. *Proc. Natl. Acad. Sci. U. S. A.* **2013**, *110*, 4200–4205.
- (50) Chen, M.; Zheng, L.; Santra, B.; Ko, H.-Y.; DiStasio, R. A., Jr.; Klein, M. L.; Car, R.; Wu, X. Hydroxide diffuses slower than

hydronium in water because its solvated structure inhibits correlated proton transfer. *Nature Chem.* **2018**, *10*, 413–419.

(51) Calle-Vallejo, F.; Martínez, J. I.; García-Lastra, J. M.; Sautet, P.; Loffreda, D. Fast prediction of adsorption properties for platinum nanocatalysts with generalized coordination numbers. *Angew. Chem., Int. Ed.* **2014**, *53*, 8316–8319.

(52) Calle-Vallejo, F.; Tymoczko, J.; Colic, V.; Vu, Q. H.; Pohl, M. D.; Morgenstern, K.; Loffreda, D.; Sautet, P.; Schuhmann, W.; Bandarenka, A. S. Finding optimal surface sites on heterogeneous catalysts by counting nearest neighbors. *Science* **2015**, *350*, 185–189.

(53) Jørgensen, M.; Grönbeck, H. Scaling Relations and Kinetic Monte Carlo Simulations to Bridge the Materials-Gap in Heterogeneous Catalysis. *ACS Catal.* **2017**, *7*, 5054.

(54) Adams, J. S.; Kromer, M. L.; Rodríguez-López, J.; Flaherty, D. W. Unifying concepts in electro- and thermocatalysis toward hydrogen peroxide production. *J. Am. Chem. Soc.* **2021**, *143*, 7940–7957.

Recommended by ACS

Improving the Hydrogen Oxidation Reaction Rate of Ru by Active Hydrogen in the Ultrathin Pd Interlayer

Xianmeng Song, Feng Ru Fan, *et al.*

JUNE 02, 2023
JOURNAL OF THE AMERICAN CHEMICAL SOCIETY

READ 

Size-Dependent Energy and Adhesion of Pd Nanoparticles on Graphene on Ni(111) by Pd Vapor Adsorption Calorimetry

Kun Zhao, Charles T. Campbell, *et al.*

FEBRUARY 07, 2023
ACS CATALYSIS

READ 

Ultralong Distance Hydrogen Spillover Enabled by Valence Changes in a Metal Oxide Surface

Taro Kamada, Yuichi Shimakawa, *et al.*

JANUARY 10, 2023
JOURNAL OF THE AMERICAN CHEMICAL SOCIETY

READ 

Colloidally Engineered Pd and Pt Catalysts Distinguish Surface- and Vapor-Mediated Deactivation Mechanisms

Jinwon Oh, Matteo Cargnello, *et al.*

JANUARY 17, 2023
ACS CATALYSIS

READ 

Get More Suggestions >